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High yield synthesis of multi-walled carbon nanotubes by catalytic decomposition of ethane over iron supported on alumina catalyst

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Abstract

Ethane was successfully used as an active and efficient carbon source in a large scale synthesis of high quality carbon nanotubes by chemical vapour deposition (CVD) over Fe/Al₂O₃ catalyst with an iron loading of 20 wt.%. The multi-walled carbon nanotubes yield approaching 50 g per gram of catalyst per hour at 750 °C, which was among the highest yield reported today in the open literature. The active phase for growing carbon nanotubes is a mixture of a metastable iron carbide (Fe₃C) and α -Fe which were formed in situ by the ethane dissociation followed by carbon diffusion through the starting α -Fe phase. The reaction products only contained multi-walled carbon nanotubes with very homogeneous diameters of around 30 nm and lengths up to several hundred nanometers without any trace of other impurities such as nanoparticles or amorphous soot. According to the observed results ethane is an active carbon source for growing multi-walled carbon nanotubes with high yield and selectivity. The reaction temperature should be keep \leq 750 °C as synthesis carried out at 800 °C under similar reaction conditions led to the formation of amorphous soot and carbon nanoparticles mixed with nanotubes. © 2005 Elsevier B.V. All rights reserved.

Keywords: Carbon nanotubes; Multi-walled; Chemical vapour deposition; Catalytic decomposition of ethane

1. Introduction

Carbon nanofilaments, either nanotubes or nanofibers, have received increasing scientific and industrial interest during the last two decades owing to their exceptional physical and chemical properties [1,2]. These nanostructured carbon materials belong to a new class of support for use in several catalytic domains, i.e. gas- and liquid-phase processes, with catalytic performances often higher than that encountered over traditional grain-shaped catalysts.

Large scale syntheses of carbon nanostructures, nanotubes and nanofibres, are today mainly conducted through a catalytic route due to the high yield, high selectivity and low cost [3,4], when compared to the traditional physical routes

such as laser ablation or arc-discharge [5–9]. Moreover, the control of the nanostructure morphology can be accurately realized through the tuning of the reaction parameters and the catalyst composition. The high selectivity of the catalytic method towards the formation of carbon nanostructures also avoids the need for a post-purification step, which is a time and cost-consuming process. Despite the significant amount of research, which has been initiated on this subject, the large scale synthesis of nanostructured materials with high purity for potential applications is still being investigated. In three recent studies, the reaction and synthesis parameters of carbon nanotubes, relatively high yields were reported [8–11]. A high yield of multi-walled carbon nanotubes by fluidized bed has also been reported by Corrias et al. [12].

The aim of the present work is to report the large scale, i.e. several grams per hour, synthesis of multi-walled carbon nanotubes (MWNTs) with a uniform diameter by the

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chemical vapour deposition (CVD) method over Fe supported on alumina at relatively low temperature, i.e. 750 °C, using a synthesis mixture consisting of ethane and hydrogen in an appropriate ratio. Ethane was preferred as carbon source as because, already reported by our group, ethane allows the synthesis of carbon nanofibers with a significant yield, i.e. 50 g per gram of nickel per hour [13,14]. One of the highest reported in the open literature to date. Ethane is also a cheap and non-toxic carbon source compared to other gaseous carbon sources. The quality and the microstructure of the carbon nanotubes were investigated by scanning electron and transmission electron microscopy.

2. Experimental

The support used was a high surface area γ-Al₂O₃ (CK 300B Ketjen with a surface area of 220 m² g⁻¹), which was mainly made up of a mesoporous network. The alumina support was crushed and sieved and a fraction of 80–150 µm was retained for catalyst preparation. The catalyst was prepared using an aqueous solution of Fe (Fe(NO_3)₃·9H₂O), with the Fe concentration fixed at 20 wt.%. The iron loading was measured by means of the ICP-MS method (Laboratoire Central d'Analyse, CNRS) and was amounted to 18.9 wt.%. The wet solid was dried at 100 °C and then calcined in air at 450 °C for 2 h in order to obtain the oxidic form of the catalyst precursor. The catalyst (0.06 g), in its oxidic form, was placed in a ceramic boat inside a quartz tube (diameter, 30 mm; length, 600 mm), located in a horizontal electrical furnace, and flushed for 30 min in flowing hydrogen at room temperature and finally reduced at 650 °C for 2 h. After this treatment the hydrogen flow was replaced by a mixture of ethane and hydrogen (60:60 ml min⁻¹) and the temperature of the furnace was rapidly increased (20 °C min⁻¹) to 750 °C. The synthesis was carried out at 750 °C for 2 h. After synthesis the raw products were treated with a solution of KOH (1 M) at 80 °C in order to remove the alumina support. The resulting material was washed several times with distilled water and then treated with a solution of HCl (1 M) in order to remove the remaining iron particles, it was then washed with distilled water before being dried at 200 °C.

Carbon yields were calculated by weighing the sample after the reduction process and after the carbon nanotube synthesis according to the following formula:

CNTs yield (wt.%) =
$$\left[\frac{(M_{\rm F} - M_{\rm I})}{M_{\rm I}}\right] \times 100$$

where $M_{\rm F}$ is the total weight obtained after synthesis, $M_{\rm I}$ is the weight of the catalyst after reduction.

The re-oxidation of the iron active phase during weighting of the sample can be neglected as the main part of the iron was encapsulated by a layer of carbon and was no longer exposed to oxygen.

X-ray diffraction (XRD) patterns of powdered samples were recorded at room temperature using a Siemens D-5000 diffractometer with a Cu K α non-monochromatic radiation source (λ = 1.54056 Å). Scanning electron microscopy (SEM) was performed on a JEOL 6700F microscope with an accelerated voltage of 3 kV. Transmission electron microscopy (TEM) was carried out on a Topcon 002B-UHR microscope working under an accelerated voltage of 200 kV and with a point-to-point resolution of 0.17 nm. Surface area was measured using a Coulter SA-3100 sorptometer with N_2 as adsorbant at liquid nitrogen temperature. Before measurement the samples were outgased at 200 °C for 2 h in order to desorb moisture and other weakly adsorbed residues.

3. Results and discussion

3.1. SEM characterisation

The morphology of the As-synthesized carbon nanostructures was investigated by SEM. The SEM images show the presence of a homogeneous distribution of carbon nanotubes covering the alumina-based catalyst surface in a web-like network. The purified sample shows that the carbon nanotubes were homogeneous in diameter, ca. 30 nm, and with lengths up to micrometers resulting in an average aspect ratio >50.

Statistical SEM observation revealed that the selectivity towards carbon nanotubes was extremely high and no traces of onion-like or carbon particles were observed in the sample. The selective growth of carbon nanotubes requires a perfect balance between the rate of carbon supply and that of solid carbon precipitation otherwise amorphous carbon can build-up on the catalyst surface leading to deactivation and the formation of impurities.

The carbon nanotubes obtained by the CVD method are less straight than those obtained by physical methods such as arc-discharge or laser ablation. This is attributed to the low temperature synthesis used in the CVD method, which favours the formation of structural defects responsible for the bending or twisting of the tubes. However, a high synthesis temperature, i.e. 800 °C instead of 750 °C, keeping other reaction conditions similar led to the formation of carbon particles instead of carbon nanotubes as shown in Fig. 1 where a mixture of nanotubes and nanoparticles was observed. It is expected that at high reaction temperature part of the carbon gaseous source was directly underwent pyrolysis leading to the formation of carbon nanoparticles or turbostratic structure instead to be transformed into carbon nanotubes.

3.2. TEM characterisation

The low magnification TEM image (Fig. 2A) shows that the carbon nanotubes were the only product obtained and no

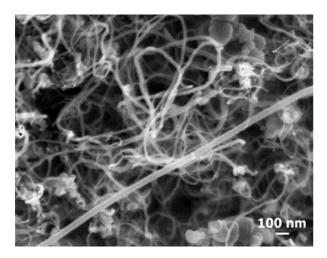


Fig. 1. SEM image of a mixture of carbon nanotubes and carbon nanoparticles synthesized at $800\,^{\circ}$ C in the presence of C_2H_6 and H_2 mixture. The high temperature of synthesis also leads to the formation of MWNT with different diameter.

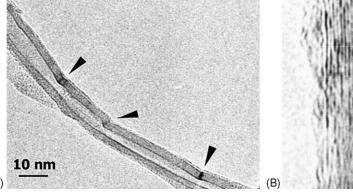
trace of carbon nanoparticles (less than 1–2%) according to the statistical TEM observation, was observed in the sample, which indicated the high selectivity of the synthesis method in good agreement with the SEM results. TEM observation also showed that some tubes were bent where defects occurred during the growth, leading to a change in the growth direction. The carbon nanostructures were MWNTs with diameters ranging from 15 to about 50 nm and lengths up to several hundred nanometers leading to an aspect ratio >50. High-resolution TEM image shows that the nanotubes were made of parallel graphene planes oriented along the tube axis and only a very small amount of amorphous carbon was observed on their outer surfaces (Fig. 2B). The amorphous carbon originated from the pyrolysis of the hydrocarbon during the cooling of the system; this is frequently reported in the CVD synthesis [9]. This phenomenon could be avoided or diminished by rapid evacuation of the reaction atmosphere at the end of the synthesis as reported by Emmenegger et al. [9]. The

interplanar distance between two adjacent graphene planes was about 0.34 nm, which is close to that of the [0 0 2] interplanar distance in graphite, i.e. 0.335 nm. The higher interplanar distance observed on the MWNTs was attributed to the curved shape of their structures, which induce strain inside the graphene planes stacking [1]. Due to the low reaction temperature some defects could be observed between the graphene planes (indicated by arrows in the Fig. 2A).

The bamboo-like or nanoparticles of carbon were completely absent from the sample and only tubes, more or less straight, were observed. This could be attributed to the interactions between the deposited iron phase and the support. Ermakova et al. [15] have reported that during the synthesis of MWNTs over iron supported on TiO₂ several types of carbon nanofilaments, i.e. straight, bamboo-like or nanoparticles, were observed. On the other hand, when TiO₂ was replaced by SiO₂ a smaller number of bamboo-like carbon structure was observed. The interaction between the active phase and the support explain these results.

Careful high-magnification TEM revealed the presence of nanotubes both with an open and with a closed tips (Fig. 3). No iron metal particles were observed on the tube tips indicating that the main growth mode followed a base growth mechanism [16]. Some iron particles were observed inside the carbon nanotube bodies (arrow in Fig. 3), which indicate that during the growth process some iron was carried out of the support surface by the tube growth. The nature of the iron particle encapsulated inside the MWNT was checked by EDS with an electron bean of 4 nm.

It is thought that during the carbon diffusion process through the iron lattice an elevation of temperature occurred causing oscillation of the lattice and a rise in temperature. As a result, the iron was transformed from the solid state into a quasi-liquid state despite the fact that the synthesis temperature was far lower than the melting temperature of iron [15]. The quasi-liquid iron phase was extracted during the MWNT growth and, remained in a encapsulated iron phase within the carbon nanotube channel and thus, was



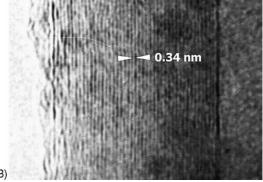


Fig. 2. TEM images of the MWNTs with different magnifications. The low-magnification image (A) reveals the presence of some structural defects along the tube axis (arrow). The high-resolution image (B) clearly shows the stacking of the graphene basal planes parallel to the tube axis. The graphene planes were not perfectly parallel and some defects can be observed (indicated by arrows).

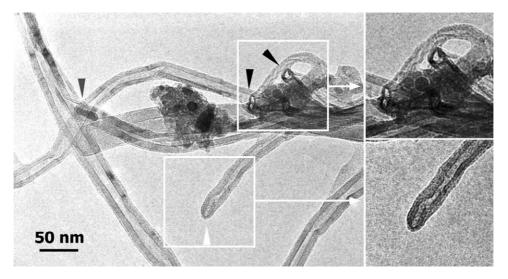


Fig. 3. TEM image of MWNTs synthesized by the CVD method with open (black arrows) and closed (withe arrow) tube tips. The presence of some encapsulated iron inside the tubes was also observed (grey arrow).

unaccessible for the further MWNT growth resulting to a gradual loss of the MWNT production with time on stream. A similar mechanism of MWNT growth over iron-based catalyst has been proposed by Ermakova et al. [15]. This encapsulation process provides an explanation why the yield of carbon nanotubes was significantly lower than the yield of carbon nanofibers over a nickel catalyst where almost no fragmentation was ever observed. Park and Keane [17] have recently reported that during the growth of carbon nanofibers from a nickel catalyst some nickel fragmentation was also observed. However, this phenomenon was observed with a significant lesser extent than that seen with the iron phase.

3.3. Specific surface area measurements

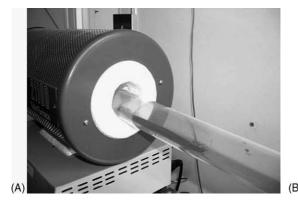
The specific surface area of the MWNTs after the purification steps was between 100 and $160~\text{m}^2~\text{g}^{-1}$ depending on the synthesis conditions. The specific surface area was titeny influenced by several synthesis parameters: (i) synthesis temperature, (ii) synthesis duration, (iii) nature and space velocity of the reactants. This was close to the data reported in

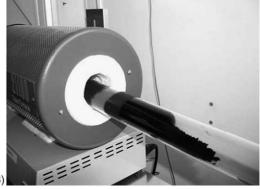
the literature as in general the surface area of the MWNTs determined by BET techniques is 20 to 100 m² g⁻¹ ranging between the surface area of graphite and of activated porous carbons [1]. It is worth noting that the measured specific surface area was mainly linked with a mesoporous network as no trace of micropore was observed among the sample.

3.4. MWNT yield as a function of the synthesis duration

According to the calculation already described a carbon nanotube yield of 20 g of carbon nanotubes per gram of catalyst, was obtained over the Fe-20 wt.%/Al₂O₃ catalyst at temperature ranging from 650 to 720 °C. Optical micrographs of the starting catalyst and the final product are presented in Fig. 4 to illustrate the possibility to synthesize MWNT with high purity and yield. Work is ongoing to check the influence of the synthesis conditions, i.e. temperature, flow rate and duration, and the concentration of the gaseous carbon source on the total MWNT yield.

The nucleation of filamentous carbon requires a supersaturation of carbon in iron, followed by a phase





 $Fig.\ 4.\ Experimental\ set-up\ for\ carbon\ nanotubes\ synthesis:\ (A)\ Fe/Al_2O_3\ catalysts\ before\ MWNTs\ synthesis\ and\ (B)\ MWNTs\ produced\ after\ synthesis.$

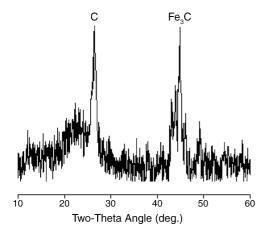


Fig. 5. XRD patterns of Fe-supported catalyst after carbon nanotubes growth synthesis.

transformation of the starting iron into Fe₃C and precipitation of carbon layers at the metal-support interface to yield carbon nanotubes. The XRD pattern of the catalyst reduced at 650 °C and subsequently reacted under a mixture of C₂H₆ and H₂ is reported in Fig. 5 where the diffraction line corresponding to the [0 0 0 2] plane of graphite was clearly visible at $\theta = 23.5^{\circ}$ and the presence of Fe₃C phase after synthesis of carbon nanotubes. The Fe₃C phase has been known to be an active phase for the carbon nanotubes formation [3,18]. According to the proposed mechanism the nature of the gaseous hydrocarbon plays an important role in the final yield: the degree of supersaturation is generally determined by the affinity for carbon formation of the gasphase. The nature of the metal-support interface also strongly influences the rejection or precipitation of carbon at this interface. Iron supported on silica catalyst was more active for carbon nanotube formation than iron supported on silicon carbide despite the similarity in the precursor phase nature. The carbon nanotube growth and selectivity were also strongly governed by the reaction temperature for a given reactant mixture and a given catalyst. In the presence of a mixture of ethane and hydrogen the optimal synthesis temperature for high quality carbon nanotubes was around 750 °C. At a higher temperature, i.e. 800 °C, carbon nanotubes of lower quality were obtained, i.e. nanotubes and amorphous carbon (not shown). Apparently, at high reaction temperature the rate of hydrocarbon decomposition and amorphous carbon formation were high enough to overcome that of the MWNT growth.

It was expected that when C_2H_6 was used as carbon source the number of carbon nuclei formed on the catalyst surface would significantly increase compared to those formed on silica or carbon supports, which in turn would accelerate the rate of carbon diffusion from the carbide surface to the carbide-support interface where carbon nanotubes were precipited. The solubility of carbon in the iron carbide surface significantly differed from the equilibrium value at the carbide-support interface and therefore a driving force for the diffusion of carbon through

the iron carbide particles was initiated, leading to continuous growth of the carbon nanotubes with the concomitant formation of $\alpha\textsc{-}\mbox{-}\mbox{Fe}$ which allowed further decomposition of the hydrocarbon to yield carbon for subsequent tube growth. Yang et al. [19] have reported that the carbon concentration near the nickel particles in contact with a mixture of methane and hydrogen was 35% higher than for a mixture in equilibrium with graphite.

4. Conclusion

In summary, C_2H_6 seems to be an appropriate carbon gaseous source for growing multi-walled carbon nanotubes selectively and with a high yield using the CVD method at the relatively low temperature of $650-750\,^{\circ}\text{C}$. The selectivity of the carbon nanotubes synthesized in the present work was high, avoiding the need for a costly purification step to eliminate by-products, as generally encountered with physical methods such as arc-discharge or laser ablation. According to the present synthesis several grams of pure MWNTs with homogeneous diameters of about 30 nm were obtained on the basis of 1 g of catalyst after 4 h of reaction at 750 $^{\circ}\text{C}$.

The possibility to synthesize carbon nanotubes with high selectivity and quality in mild conditions makes them more appealing for use in other applications where the exceptional physical and chemical properties of these materials would be of great benefit. Work is on-going to evaluate the catalytic properties of these nanomaterials in several gas and liquid-phase reactions, and also to study the influence of the nature of the active phase and the support on the final carbon nanotubes yield.

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References

- [1] P.M. Ajayan, Chem. Rev. 99 (1999) 1797.
- [2] H.J. Dai, Acc. Chem. Res. 35 (2002) 1045.
- [3] M. Pérez-Cabero, I. Rodriguez-Ramos, A. Guerrero-Ruiz, J. Catal. 215 (2003) 305.
- [4] S. Tang, Z. Zhong, Z. Xiong, L. Sun, L. Liu, J. Lin, Z.X. Shen, K.L. Tan, Chem. Phys. Lett. 350 (2001) 19.
- [5] X. Zhao, M. Ohkohchi, H. Shimoyama, Y. Ando, J. Crystal Growth 198 (1999) 934.
- [6] J.M. Bonard, L. Forro, D. Ugarte, W.A. de Heer, A. Châtelain, ECC Res. 1 (1998) 9.
- [7] T.W. Ebbesen, P.M. Ayajan, Nature 358 (1992) 220.
- [8] Ph. Mauron, C. Emmenegger, A. Züttel, C. Nützenadel, P. Sudan, L. Schalapbach, Carbon 40 (2002) 1685.

- [9] C. Emmenegger, J.-M. Bonard, P. Mauron, P. Sudan, A. Lepora, B. Grobety, A. Zuttler, L. Sschapbach, Carbon 41 (2003) 539.
- [10] P. Mauron, C. Emmenegger, P. Sudan, P. Wagner, S. Rentsch, A. Zuttler, Diam. Rel. Mater. 12 (2003) 780.
- [11] N. Nagaraju, A. Fonseca, Z. Konya, J.B. Nagy, J. Mol. Catal. A: Chem. 181 (2002) 57.
- [12] M. Corrias, B. Caussat, A. Ayral, J. Durand, Y. Kihn, Ph. Kalck, Ph. Serp, Chem. Eng. Sci. 58 (2003) 4475.
- [13] R. Vieira, C. Pham-Huu, N. Keller, M.J. Ledoux, Chem. Commun. (2002) 954.
- [14] C. Pham-Huu, N. Keller, V.V. Roddatis, G. Mestl, R. Schlögl, M.J. Ledoux, Phys. Chem. Chem. Phys. 4 (2002) 514.
- [15] M.A. Ermakova, D.Y. Ermakov, A.L. Chuvilin, G.G. Kuvshinov, J. Catal. 201 (2001) 183.
- [16] C. Laurent, E. Flahaut, A. Peigney, A. Rousset, New J. Chem. 1 (1998) 229, and references therein.
- [17] C. Park, M.A. Keane, J. Catal. 221 (2004) 386.
- [18] J.W. Snoeck, G.F. Froment, M. Fowles, J. Catal. 169 (1997) 240.
- [19] R.T. Yang, P.J. Goethel, J.M. Schwartz, C.R.F. Lund, J. Catal. 122 (1990) 206.